

ARCHIVE 2006 Session 7

Thermal Management Advances

"DUT Thermal Management - An Overview Of Applied Passive Thermal Control Technology For Integrated Circuit Test" F. D. Boatright — Delta Design, Inc.

"Thermal Control Units: Development Of An Analytical Model And Experimental Validation To Optimize The Voltage Input" Sudhir Kumar, Khaled Elmadbouly, Praba Prabakaran Kulicke & Soffa Industries

"Using A High Performance Micro-channel Cold Plate For Test And Burn-in" Zahed Sheikh — Mikros Technologies

"Managing The Thermal Budget During Burn-In – A New Concept For Control" Chris Lopez, Dr. James Forster, Trevor Moody UMD Advanced Test Technologies

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Comparison of DUT Air Impingement and Contactor **Probe Conditioning Thermal Contactor:** 125°C Air Injection - 30SCFH Purge 140 135 130 125 120 115 110 105 100 95 90 85 80 75 70 65 60 **Average Insertion Loss** @2°C w/ 45°C Gradient 125°C Thermal Contactor - 30SCFH Purge $\begin{array}{c} 140\\ 135\\ 130\\ 125\\ 120\\ 115\\ 110\\ 105\\ 100\\ 95\\ 90\\ 85\\ 80\\ 75\\ 70\\ 65\\ 60\\ \end{array}$ Time = 10 Samples/Sec A1 Dev Z3 RTD Ref Z3 Mtg Plate A -B1 Dev - B2 Dev LDBD 1 LD Air Injection: Average Insertion Loss Time = 10 Samples/Sec @11°C w/ 45°C Gradient Z3 RTD Ref A2 Dev _____B2 Dev ____LDBD 1 ____LDBD 2 Z3 Mtg Plate Page 10

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Dynamic Test Results Using Embedded RTD Test Vehicles







 Summary of Approaches and Conclusions

 Contactor Probe Conditioning

 • Optimal in minimizing transient effects from temperature mismatches from the DUT contacts and test probes.

 DUT Applied Thermal Load

 • In the convection mode, a small contributor to overcoming the heat transfer effects from the socket and loadboard.

 DIB Cover (Purge Cap)

 • Effective in maintaining the gradient across the contactor probes and loadboard.

 Eliminates extraneous air currents induced by test head purge and test cell environment.

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Thermal Control Units: Development of an Analytical Model and Experimental Validation to Optimize the Voltage Input

Sudhir Kumar (Presenter), Khaled Elmadbouly, Praba Prabakaran



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Analytical Model	Sub-Assemblies Details	
Heat transfer analysis is done for the water chiller to determine the average water temperature.	$egin{aligned} \mathbf{Q}\mathbf{h} &= \mathbf{x}\mathbf{\hat{v}} \star \mathbf{C}\mathbf{p} \star (\mathbf{T}_{water, out} - \mathbf{T}_{water, in}) \ \mathbf{T}_{water, av} &= rac{\mathbf{T}_{water, in} + \mathbf{T}_{water, out}}{2} \end{aligned}$	
The internal thermal resistance of the TEC is also calculated and taken into account.	$R_{\text{TEC}} = R_{\text{Alumina}} + R_{\text{Copper}} + R_{\text{Solder}}$ $Qc = 2 \star Q$	
One dimensional thermal resistance models of the sub-assemblies are developed and integrated with the TEC model.	$P = V * I$ $Power = 2 * P$ $Qh = Qc + Power$ $Qc * (\frac{R_{TEC}}{2} + Rc + R_1 + R_2) = T_{Die} - Tc$ $Qh * (\frac{R_{TEC}}{2} + Rh) = Th - T_{water, av}$	
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Conclusions

- The system level model of the TCU is used to determine the variation of the die junction temperature versus the TEC operating voltage for the heat loads of 50 W and 140 W. It was found that the optimal voltage input is 19 V per TEC.
- Subsequently, experimental validation is done and it is observed that simulation results of the model are quite accurate. The optimal voltage is found to be 19 V per TEC experimentally also.
- Besides die temperature, variation of other parameters like electric power, COP with respect to TEC voltage was also studied for the heat loads of 50 W and 140 W.

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Using a High Performance Micro-channel Cold Plate for Test and Burn-in



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Presentation Topics

- Issues in Temperature Control during Test and Burn-in
- ➢ Current Solutions
- Flow-based control
- Normal Flow Micro-channel







Maintaining T_j for High Power Devices

$$T_{J} = T_{in} + q'' \Big[R_{flow}^{"} + (R_{core}^{"} + R_{TIM}^{"} + R_{d}^{"}) \Big]$$

$$R_{cp}^{"} = R_{flow}^{"} + R_{core}^{"} \qquad \text{Core Resistivity}$$

$$R_{flow}^{"} = \frac{1}{m''Cp} \qquad \text{Flow Resistivity}$$
If the core resistivity is small, then the cold plate thermal resistivity is inversely proportional to the flow rate
$$P_{low}^{"} = P_{low}^{"} + R_{core}^{"} \qquad P_{low}^{"} + P_{core}^{"} + P_{c$$



Temperature Variation in a Burnin Chamber

- Variation in T_i leads to longer BI time
- Tight T_i distribution increases yield
- > Sources of variation:
 - Variation in inlet T to the cold plate
 - Variation in power dissipation of components
 - Variation in the thermal resistance of the device and the interface
 - Variation in the CP/HS thermal resistance





























Normal Flow Pressure Drop

$$R_{core,\min}^{"} = \frac{g}{\sqrt{2k_s k_f}}$$
$$\Delta P \propto \frac{L}{g} V$$

For parallel flow L (channel length) is constant and V is inversely proportional to the gap size. So, $\Delta P \propto \frac{1}{g^2}$

For normal flow, the flow path is H, the channel height.

$$\Delta P \propto \frac{H}{g} V$$

In normal flow arrangement, V is constant and H is proportional to g so ΔP stays constant























Conclusions

- A cold plate based on the Normal Flow Technology has very low thermal resistance
- For the proper ranges of the interface and device resistance, the junction to ambient resistance can be controlled by varying the flow rate through the cold plate
- They key to successful control remains to be a low value of interface resistance
- Normal Flow arrangement lends itself to managing hot spots

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"The Cost of Test is Approaching the Cost of Silicon"

-Senior Semiconductor Manager

"Google's Energy Bill for its Servers Now Exceeds the Cost of the Equipment."

-Business Week Online

Thermal Management

Definition

 The art by which heat is controlled and removed by various means such as air or liquid and carried to an alternate location

The First Law of Thermodynamics (Conservation) states that energy is always conserved, it cannot be created or destroyed. In essence, energy can only be converted from one form to another.

Managing the Thermal Budget During Burn-In – A New Concept for Control – Lopez et al.

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- Conventional Burn-in chambers
 - Box with recirculating air, usually cooled by air-to-air or air-to-liquid heat exchangers
 - Thermal Management consists of adding as big of a heat sink as possible (typically)

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Technology Drivers

- Increase yields
- Maximize visibility
- Eliminate the need for sort
- Maximize utilization
- Meet increasing demands of higher power, higher variance devices

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The Problem

- Today's batch process is becoming a thing of the past for even low power devices
- Because of wide power variations in today's products devices need to be binned in order to be processed in conventional burnin systems
- Binning is inefficient and economically bad
 - Throughput suffers
 - The bins are not always apparent up front

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Managing the Thermal Budget During Burn-In – A New Concept for Control – Lopez et al.

The Problem • Device - 10W nominal logic device Integrated heat spreader Conventional Burn-In - .4 C/W Package Resistance – 1.2 C/W Interface Resistance - 1.5 C/W Heat Sink Resistance @ 800 lfm (Chamber Spec.) - Total = 3.1 C/W - 31 C rise – Set chamber to 94 C Device running at 125 C junction temperature • Sounds Easy... Managing the Thermal Budget During Burn-In – A New BiTS Workshop - 2006 16 Concept for Control - Lopez et al.





The Problem			
 Conventional Reality Device Varies from 5W to 15W .4 C/W Package Resistance 1.2 C/W Interface Resistance 1.5 C/W Heat Sink Resistance @ 800 lfm (Chamber Spec.) Total = 3.1 C/W 15 C rise to 46 C rise Set chamber to ??? C Device running at ??? C junction temperature The "other" factors What about airflow variances? What about devices heating up downstream devices? And oh yeah and all these calculations are at room temperature as device heats up so does the variance 			
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Advanced Thermal Management

- We could...
 - Liquid cooling
 - Expensive
 - Prohibitive upfront capital expenditure
 - Dedicated
 - Maintenance Heavy
 - Impinged air active control systems
 - Expensive
 - Prohibitive upfront capital expenditure

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- Low Density
- Consumables at a high cost

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